

### **What is Desalination?**

Areas that have either no or limited surface water or groundwater may choose to desalinate water. Reverse osmosis is an increasingly common method of desalination, because of its relatively low energy consumption.

In recent years, energy consumption has dropped to around 3 kWh/m<sup>3</sup> with the development of more efficient energy recovery devices and improved membrane materials. According to the International Desalination Association, for 2011, reverse osmosis was used in 66% of installed desalination capacity (0.0445 of 0.0674 km<sup>3</sup>/day), and nearly all new plants.

Other plants mainly use thermal distillation methods: multiple-effect distillation and multi-stage flash.



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Sea water RO desalination process has been commercially used since 1970s. Energy requirement is low comparison to other processes of desalination such as 2,2 kWh/m<sup>3</sup>. Up to %50 of the seawater input can be recovered as fresh water.

**Typical SWRO System consists of;**

- \* Intake (Deep well, beach well, open intake, deep sea intake...)
- \* Pre-treatment (multimedia filter, cartridge filter, dosing units...)
- \* High pressure pump (according to calculated required pressure with or without energy recovery unit)
- \* Membrane assembly (according to design program)
- \* Energy recovery (details are below)
- \* Remineralization (dolomite filter...)
- \* Disinfection (ultraviolet or chlorine dosing)



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## **Pretreatment**

Pretreatment is important when working with reverse osmosis membranes due to the nature of their spiral wound design. For SWRO pretreatment has four major components.

- multimedia filtration
- cartridge filtration
- chemical dosing (smbs, antiscalant...)
- pH adjustment

## **High Pressure Pump**

The high pressure pump supplies the pressure needed to push water through the membranes, even as the membrane rejects the passage of salt through it. For SWRO system pressure required is changing from 30 bar to 80 bars.



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## Membrane Assembly

The membrane assembly consists of a pressure vessel with a membrane that allows feedwater to be pressed against it. The membrane must be strong enough to withstand whatever pressure is applied against it. Reverse osmosis membranes are made in a variety of configurations, with the two most common configurations being spiral-wound and hollow-fiber.

Only a part of the saline feed water pumped into the membrane assembly passes through the membrane with the salt removed. The remaining "concentrate" flow passes along the saline side of the membrane to flush away the concentrated salt solution.

The percentage of desalinated water produced versus the saline water feed flow is known as the "recovery ratio".

This varies with the salinity of the feed water and the system design parameters: typically 20% for small seawater systems, 40% – 50% for larger seawater systems, and 80% – 85% for brackish water.





The concentrate flow is at typically only 3 bar / 50 psi less than the feed pressure, and thus still carries much of the high pressure pump input energy.

### **Energy Recovery**

Energy recovery can reduce energy consumption by 50% or more. Much of the high pressure pump input energy can be recovered from the concentrate flow, and the increasing efficiency of energy recovery devices has greatly reduced the energy needs of reverse osmosis desalination. Devices used, in order of invention, are:

- Turbine or Pelton wheel: a water turbine driven by the concentrate flow, connected to the HPP drive shaft to provide part of its input power. Positive displacement axial piston motors have also been used in place of turbines on smaller systems.
- Turbocharger: a water turbine driven by the concentrate flow, directly connected to a centrifugal pump which boosts the high pressure pump output pressure, reducing the pressure needed from the high pressure pump and thereby its energy input, similar in construction principle to car engine turbochargers.
- Pressure exchanger: using the pressurized concentrate flow, in direct contact or via a piston, to pressurize part of the membrane feed flow to near concentrate flow pressure. A boost pump then raises this pressure by typically 3 bar / 50 psi to the membrane feed pressure. This reduces flow needed from the high-pressure pump by an amount equal to the concentrate flow, typically 60%, and thereby its energy input. These are widely used on larger low-energy systems. They are capable of 3 kWh/m<sup>3</sup> or less energy consumption.

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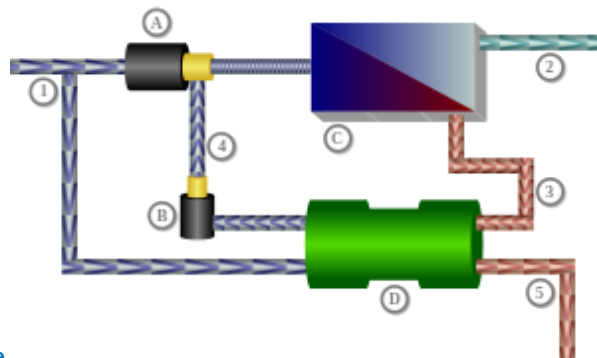
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iSave from Danfoss

Schematics of a reverse osmosis system using a pressure exchanger;

- 1: Sea water inflow,
  - 2: Fresh water flow (40%),
  - 3: Concentrate flow (60%),
  - 4: Sea water flow (60%),
  - 5: Concentrate (drain),
- A: Pump flow (40%),  
B: Circulation pump,  
C: Osmosis unit with membrane,  
D: Pressure exchanger



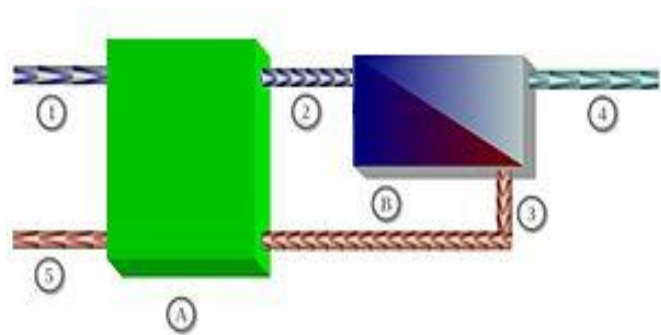
- Energy recovery pump: a reciprocating piston pump having the pressurized concentrate flow applied to one side of each piston to help drive the membrane feed flow from the opposite side.

These are the simplest energy recovery devices to apply, combining the high pressure pump and energy recovery in a single self-regulating unit. These are widely used on smaller low-energy systems.

They are capable of 3 kWh/m<sup>3</sup> or less energy consumption.

Schematic of a reverse osmosis system using an energy recovery pump;

- 1: Sea water inflow (100%, 1 bar)
- 2: Sea water flow (100%, 50 bar)
- 3: Concentrate flow (60%, 48 bar)
- 4: Fresh water flow (40%, 1 bar)
- 5: Concentrate to drain (60%, 1 bar)
- A: Pressure recovery pump
- B: Osmosis unit with membrane



- Batch operation: Reverse osmosis systems run with a fixed volume of fluid (thermodynamically a closed system) do not suffer from wasted energy in the brine stream, as the energy to pressurize a virtually incompressible fluid (water) is negligible.

Such systems have the potential to reach second law efficiencies of 60%.

## **Remineralization and pH adjustment**

The desalinated water is "stabilized" to protect downstream pipelines and storage, usually by adding lime or caustic soda to prevent corrosion of concrete-lined surfaces. Liming material is used to adjust pH between 6.8 and 8.1 to meet the potable water specifications, primarily for effective disinfection and for corrosion control.

Remineralization may be needed to replace minerals removed from the water by desalination. Although this process has proved to be costly and not very convenient if it is intended to meet mineral demand by humans and plants. The very same mineral demand that freshwater sources provided previously.



## **Disinfection**

The desalinated water is finally disinfected before the final storage tank or just after the storage tank. Ultraviolet disinfection shall be used for disinfection for better quality. As an alternative NaOCl dosing is used for disinfection.



## STANDARD SEA WATER REVERSE OSMOSIS SYSTEMS

STANDARD MODELS	Raw Water TDS < 25000	# of Membranes
100 m <sup>3</sup> /day		6
200 m <sup>3</sup> /day		12
300 m <sup>3</sup> /day		18
400 m <sup>3</sup> /day		24
500 m <sup>3</sup> /day		30
1000 m <sup>3</sup> /day		60

STANDARD MODELS	Raw Water TDS > 25000	# of Membranes
100 m <sup>3</sup> /day		8
200 m <sup>3</sup> /day		18
300 m <sup>3</sup> /day		24
400 m <sup>3</sup> /day		30
500 m <sup>3</sup> /day		36
1000 m <sup>3</sup> /day		72

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